

November 30, 2010

Mr. Andrew Fan US EPA Region III, 3WC23 1650 Arch Street Philadelphia, PA 19103-2029

Ms. Barbara Brown Project Coordinator Maryland Department of the Environment 1800 Washington Blvd. Baltimore, Maryland 21230

Re: Consent Decree, Civil Action Nos. JFM-97-558, JFM-97-559 Coke Oven Area Interim Measures Progress Report - October 2010

Dear Mr. Fan and Ms. Brown:

Enclosed with this correspondence is the *Coke Oven Area Interim Measures Progress Report October 2010* completed for the Severstal Sparrows Point Facility in accordance with the requirements outlined in US EPA's September 2, 2010 approval letter for the Coke Oven Area Interim Measures work associated with the referenced Consent Decree. The report summarizes implementation progress for the approved interim measures (IMs) that have been developed to address identified environmental conditions at the Coke Oven Area through October 31, 2010.

As of October 31, 2010, Cell 1 and Cell 6 are operational and Cell 4 is in the process of being evaluated and designed. All three Cells are addressed in this progress report. The other Cells are in various stages of evaluation, design, and under permitting considerations by Maryland Department of the Environment (MDE).

Please contact me at (410) 388-6622 should questions arise during your review of the enclosed progress report.

Sincerely,

in

Russell Becker Division Manager, Environmental Engineering and Affairs

Enclosure

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MultiMedia Consent Decree

Document Certification

Coke Oven Area Interim Measures Progress Report (October 2010)

November 30, 2010

I certify under penalty of law that this document and all attachments were prepared under my direction or supervision in accordance with a system designed to assure that qualified personnel properly gather and evaluate the information submitted. Based on my inquiry of the person or persons who manage the system, or those persons directly responsible for gathering the information, the information submitted is to the best of my knowledge and belief, true, accurate, and complete. I am aware that there are significant penalties for submitting false information, including the possibility of fine and imprisonment for knowing violations.

IMIL

Russell Becker Division Manager Environmental Engineering and Affairs

Severstal Sparrows Point LLC

COKE OVEN AREA INTERIM MEASURES PROGRESS REPORT (OCTOBER 2010)

Prepared for

Severstal-Sparrows Point, LLC Sparrows Point, Maryland





URS Corporation 200 Orchard Ridge Drive, Suite 101 Gaithersburg, MD 20878 Project no. 15302307

Introduction

In accordance with US EPA's September 2, 2010 letter, this document is the second progress report that summarizes implementation progress for the United States Environmental Protection Agency (US EPA)-approved interim measures (IMs) that have been developed to address identified environmental conditions at the Coke Oven Area (COA) Special Study Area at the Severstal Sparrows Point Facility located in Sparrows Point, Maryland. This progress report summarizes IM progress for October 2010.

For mutual ease of understanding, and as agreed during the June 3, 2010 teleconference with US EPA, the following designations are applied in this document to the six (6) IM "Cells" (**Figure 1**) at the COA:

- Cell 1: Prototype Air Sparge/Soil Vapor Extraction (AS/SVE) System in the Former Benzol Processing Area,
- Cell 2: AS/SVE and Dual Phase Groundwater Extraction System in Former Coal Storage Area,
- Cell 3: AS/SVE System in "Cove" Area,
- Cell 4: In-Situ Anaerobic Bio-treatment Area in Coal Tar Area,
- Cell 5: Groundwater Extraction at the Turning Basin Area, and
- Cell 6: LNAPL Recovery at the Former Benzol Processing Area.

As of October 31, 2010, Cell 1 and Cell 6 continue to be operational and the planned in-situ enhanced anaerobic bioremediation system at Cell 4 is in the process of being evaluated and designed. All three Cells are addressed in this progress report. The other Cells are in various stages of evaluation, design, and under permitting considerations by Maryland Department of the Environment (MDE).

Cell 1: Prototype AS/SVE System in the Former Benzol Processing Area

US EPA's March 2, 2010 letter approved the air sparge/soil vapor extraction (AS/SVE) interim measure for Cell 1, as originally proposed by Severstal. This cell consists of a prototype IM, which includes AS/SVE coupled with vapor destruction via an internal combustion engine (ICE). Design of this system includes air sparging groundwater wells and vapor collection trenches as shown schematically on **Figure 2**.

Figure 3 shows the system layout of Cell 1, which consists of the following major components:

- Three (3) generally parallel and interconnected vapor collection trenches approximately 500 feet long and 60 feet apart, fitted with perforated 4-inch DR-17 high-density polyethylene (HDPE) pipe. Fifteen (15) vertical extraction risers are connected to a common suction header,
- Sixteen (16) air sparge wells located between the trenches,
- At-grade, 4-inch DR-17 HDPE sparge and suction headers fitted with control valves for 2-inch DR-17 HDPE sparge and suction laterals,
- One (1) ICE unit for extraction vacuum and vapor destruction, which is equipped with an integral Becker KDT series air compressor for sparge air, and
- Perimeter slag berm for system demarcation and protection from vehicular traffic.

Operational performance of Cell 1 during this reporting period is summarized in **Table 1**. In summary, the ICE operated roughly 66% during this reporting period. Benzene removal rates averaged approximately 12.5 pounds per day during this period. Severstal is continuing to evaluate possible methods for enhancing benzene recovery. The ICE catalytic converter destruction efficiency has exceeded 95%.

Soil gas and ICE exhaust gas samples were collected to evaluate system performance. Calibrated field instruments (e.g., photoionization detector [PID]) and ICE system-calculated vapor concentrations were also used to evaluate system performance. The untreated soil gas samples were collected in Tedlar[®] bags and the ICE exhaust sample collected in a 6-liter SUMMA can. All gas samples were submitted to TestAmerica Laboratories, Inc. Knoxville, Tennessee laboratory for analysis by US EPA Method TO-15. These data are summarized in **Table 2**.

From **Table 2**, influent soil gas hydrocarbon concentrations, collected on October 5, 2010, was 664 parts per million by volume (ppmv). As indicated above, Severstal is evaluating measures to maximize benzene concentration in the extracted soil gas in order to maximize benzene recovery and destruction.

Groundwater samples were collected on October 29, 2010 from the following wells:

- BP-MW-09 (upgradient of Cell 1),
- CO18-PZM006 (upgradient of Cell 1 at edge of berm), and
- CO02-PZM006 (downgradient of Cell 1).

The groundwater samples were submitted to Analytical Laboratory Services, Inc. of Middletown, Pennsylvania for the analyses summarized in **Table 3**. **Table 4** presents the VOC results for the prior reporting period. These data indicate benzene is the most prevalent volatile organic compound (VOC) constituent.

Overall, Severstal is continuing to operate the prototype system and is evaluating measures to maximize hydrocarbon concentration in the extracted soil gas in order to maximize hydrocarbon recovery and destruction. These measures include:

- Performing tests to assess trench vapor capture effectiveness,
- Varying sparge air and vapor extraction locations using different configurations than previously tested,
- Varying sparge air volume and pressure at levels different than previously applied, and
- Evaluating different technologies to enhance vapor extraction.

Cell 4: In-Situ Anaerobic Bio-treatment Area in Coal Tar Area

US EPA's March 2, 2010 letter approved the in-situ bio-treatment concept for Cell 4 (**Figure 4**), as originally proposed by Severstal. As discussed in last month's progress report, baseline groundwater data and a microbial conditions evaluation using Bio-Trap[®] Samplers (Bio-Traps) were performed in July 2010 as the first step to developing a preliminary conceptual design.

Severstal is continuing efforts toward designing, installing and operating the planned in-situ enhanced anaerobic bioremediation system at Cell 4. These activities include:

- 1. Design and install a groundwater re-circulation system to deliver bionutrients to the subsurface.
- 2. Supplement the depleted nutrients that are necessary to support general microbial activities, including nitrate and phosphorous. Commercially available bionutrients (such as VB591 from BioNutra Tech) are being evaluated.
- 3. Monitor the progress of target compound degradation and microbial activities by sampling and analyzing groundwater as necessary.

Severstal is expecting to begin installation and construction activities the first quarter of 2011.

Cell 6: LNAPL Extraction at the Former Benzol Processing Area

The Cell 6 LNAPL monitoring and recovery system was monitored approximately weekly during October (five site visits). **Table 5** summarizes LNAPL occurrence and recovery observed during the reporting period and **Figure 5** illustrates the well locations.

During October, approximately 236 gallons of LNAPL was recovered, bringing the total recovered LNAPL to 1,789 gallons as of October 28. The LNAPL was recovered from the following wells:

Well	LNAPL	Notes		
wen	During October	Total thru October 28	TAULES	
BP-MW-05	166	1,550		
RW-04	61	130		
BP-MW-08	8.2	100		
BP-MW-11	0	7.8	(a)	
RW-1	1	1	(b)	

(a) Recovery system moved from BP-MW-11 to BP-MW-08 on September 8, 2010.

(b) Manual bailing.

The wells are presented in **Table 4** in the order of decreasing LNAPL occurrence/recovery. During the reporting period LNAPL has been observed in the wells listed below. Manual bailing of RW-1 was initiated on October 28.

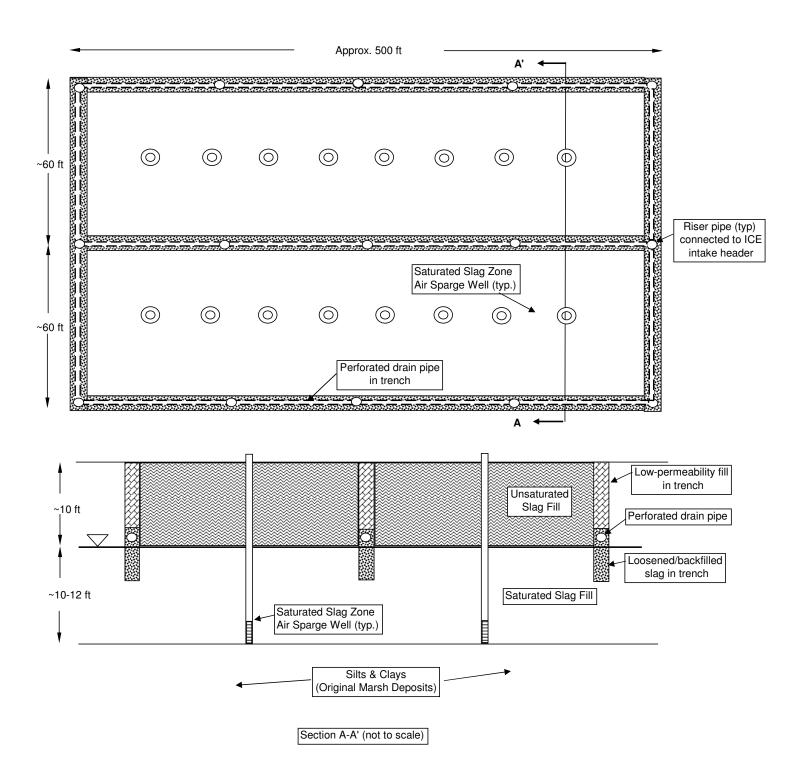
- BP-MW-11 (0.1 feet),
- BP-MW-10 (0.02 feet),
- RW-1 (0.06 to 0.95 feet),
- RW-2 (0 to 0.21 feet), and
- RW-3 (0.16 to 0.34 feet).

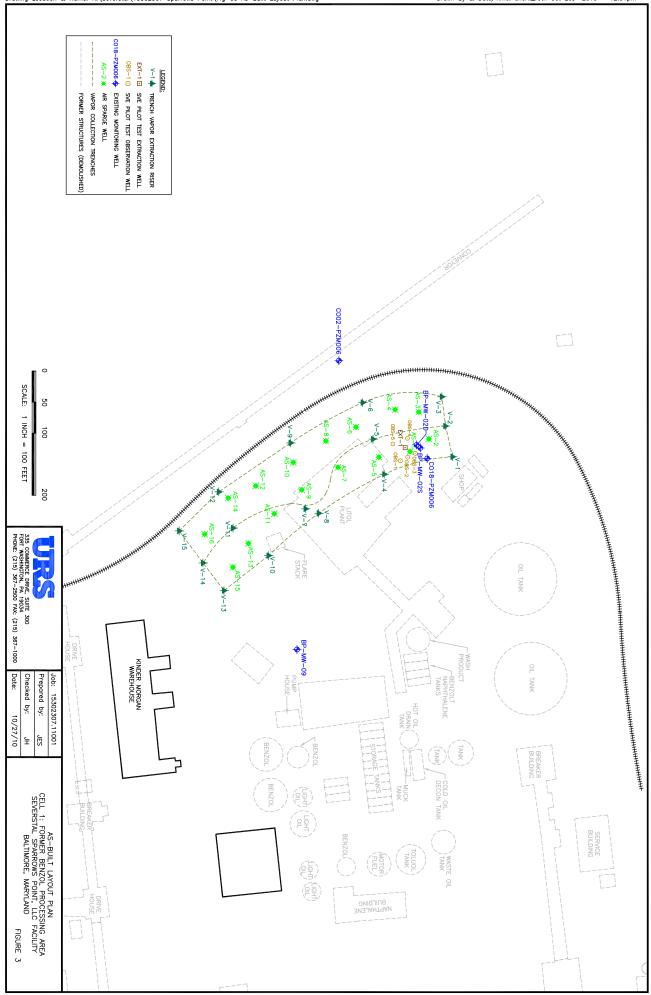
LNAPL was not observed in wells RW-5, BP-MW-07, BP-MW-06, BP-MW-09, or CO19-PZM004.

FIGURES



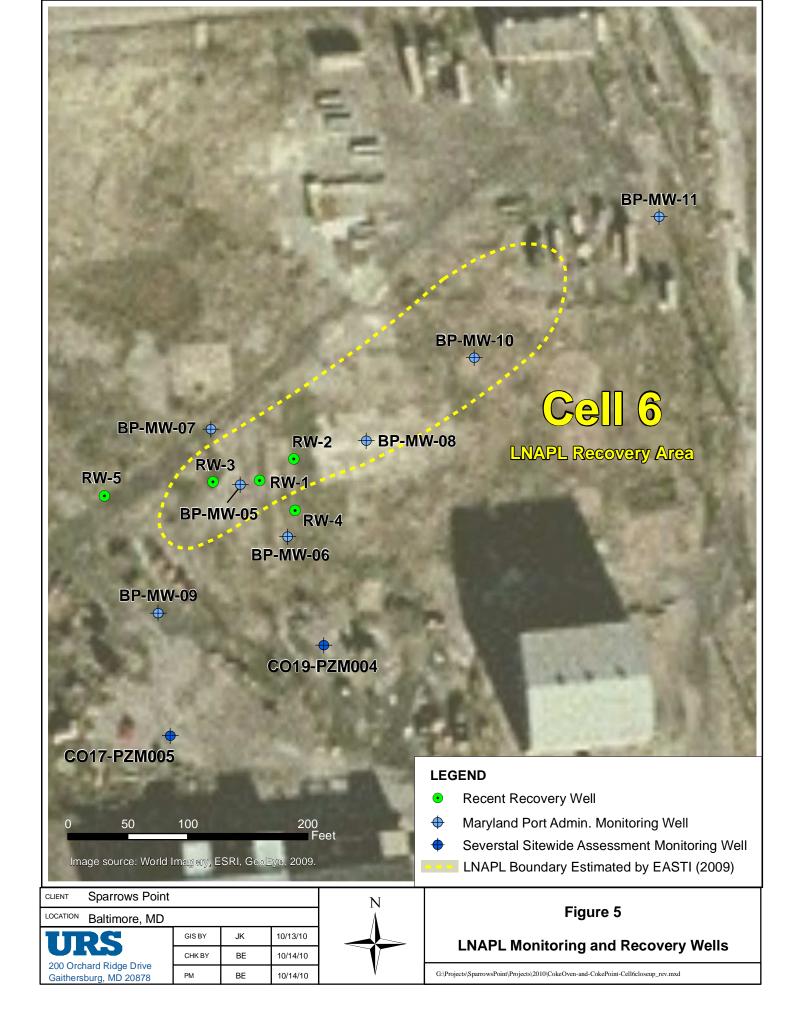
Figure 2 Schematic Diagram Cell 1: Prototype AS/SVE System in Former Benzol Processing Area Former Coke Oven Area Interim Remedial Measures Severstal Sparrows Point, LLC





	CO13 CT	-PZM0 -MW-0	€ 0BS-10 €	ZM008 OBS-6 EXT-2 AS-2 \oplus \oplus OBS BS-9 \oplus OBS-7	
				86.5	Cell 4
in the second	-	-			In-Situ Anaerobic Bio-System
0 20 Image source: World	40 Imagery, E		eet	-	
CLIENT Sparrows Point				N	[
LOCATION Baltimore, MD	1			Λ	Figure 4
URS	GIS BY	JK	10/13/10		Existing Cell 4 Wells
200 Orchard Ridge Drive	CHK BY	BE	10/14/10	- V	
Gaithersburg, MD 20878	PM	BE	10/14/10	ľ	G:\Projects\SparrowsPoint\Projects\2010\CokeOven-and-CokePoint-Cell4closeup_rev.mxd

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TABLES

Table 1Summary of Operating ConditionsCell 1: Prototype AS/SVE System in Former Benzol Processing AreaFormer Coke Oven Area Interim Remedial MeasuresSeverstal Sparrows Point, LLC

Parameter	Units	Quantity
Total ICE Operating Time (October 1 - October 31, 2010)	hours	338
Overall ICE Operational Time	%	65.8
Estimated Total Hydrocarbons Destroyed	pounds	176.2
Estimated Hydrocarbon Removal Rate	pounds/hour	0.52

Table 2

Summary of Soil Gas Analytical Results Cell 1: Prototype AS/SVE System in Former Benzol Processing Area Former Coke Oven Area Interim Remedial Measures **Severstal Sparrows Point, LLC**

	Sample ID	ICE Influent	ICE Exhaust
	Date	10/5/2010	10/5/2010
	Time	12:54	12:58
Dilut	ion Factor		1341.4
Analyte	Units		
TO-15 Volatile Organics			
trans-1,3-Dichloropropene	ppb	< 10,000 U	< 270 U
Acetone	ppb	< 250,000 U	< 6,700 U
Ethylbenzene	ppb	< 10,000 U	< 270 U
2-Hexanone	ppb	< 25,000 U	< 670 U
Methylene Chloride	ppb	< 25,000 U	< 670 U
Benzene	ppb	560,000	13,000
1,1,2,2-Tetrachloroethane	ppb	< 10,000 U	< 270 U
Tetrachloroethene	ppb	< 10,000 U	< 270 U
Toluene	ppb	71,000	1,700
1,1,1-Trichloroethane	ppb	< 10,000 U	< 270 U
1,1,2-Trichloroethane	ppb	< 10,000 U	< 270 U
Trichloroethene	ppb	< 10,000 U	< 270 U
Vinyl Chloride	ppb	< 10,000 U	< 270 U
o-Xylene	ppb	< 10,000 U	< 270 U
m-Xylene & p-Xylene	ppb	13,000	430
2-Butanone (MEK)	ppb	< 50,000 U	< 1,300 U
4-Methyl-2-pentanone (MIBK)	ppb	< 25,000 U	< 670 U
Bromoform	ppb	< 10,000 U	< 270 U
Carbon Disulfide	ppb	< 25,000 U	< 670 U
Carbon tetrachloride	ppb	< 10,000 U	< 270 U
Chlorobenzene	ppb	< 10,000 U	< 270 U
Chloroethane	ppb	< 10,000 U	< 270 U
Chloroform	ppb	< 10,000 U	< 270 U
1,1-Dichloroethane	ppb	< 10,000 U	< 270 U
1,2-Dichloroethane	ppb	< 10,000 U	< 270 U
1,1-Dichloroethene	ppb	< 10,000 U	< 270 U
trans-1,2-Dichloroethene	ppb	< 10,000 U	< 270 U
1,2-Dichloropropane	ppb	< 10,000 U	< 270 U
cis-1,3-Dichloropropene	ppb	< 10,000 U	< 270 U
Total Volatile Organics	ppb	644,000	15,130
Hydrocarbons			
Methane	%	< 0.26 U	
Notes:			

Notes: <Blank>

= Not measured

BOLD

= Analyte detected

= parts per billion

ppb </U

%

= Analyte not detected above corresponding Reporting Limit

= Percent

Table 3Summary of Groundwater Analytical ResultsCell 1: Prototype AS/SVE System in Former Benzol Processing AreaFormer Coke Oven Area Interim Remedial MeasuresSeverstal Sparrows Point, LLC

	Sample ID	CO02-PZM006	CO18-PZM006	BP-MW-09
	Date	10/29/2010	10/29/2010	10/29/2010
Analyte	Units			
Water Quality Parameters				
Temperature	deg C	20.90	22.44	18.30
pH	std units	7.97	7.32	11.7
ORP	mV	-268	-71	-387
Conductivity	mS/cm	1.370	1.950	2.380
Turbidity	NTU	15.5	5.8	3.2
DO	mg/L	0.87	0.47	0.26
Volatile Organics				
Acetone	µg/L	< 5,000 U	< 10,000 U	< 5,000 U
Benzene	µg/L	444,100	928,000	259,000
Bromoform	µg/L	< 500 U	< 1,000 U	< 500 U
2-Butanone	µg/L	< 5,000 U	< 10,000 U	< 5,000 U
Carbon Disulfide	µg/L	< 500 U	< 1,000 U	< 500 U
Carbon Tetrachloride	µg/L	< 500 U	< 1,000 U	< 500 U
Chlorobenzene	µg/L	< 500 U	< 1,000 U	< 500 U
Chloroethane	µg/L	< 500 U	< 1,000 U	< 500 U
Chloroform	µg/L	< 500 U	< 1,000 U	< 500 U
1,1-Dichloroethane	µg/L	< 500 U	< 1,000 U	< 500 U
1,2-Dichloroethane	µg/L	< 500 U	< 1,000 U	< 500 U
1,1-Dichloroethene	µg/L	< 500 U	< 1,000 U	< 500 U
trans-1,2-Dichloroethene	µg/L	< 500 U	< 1,000 U	< 500 U
1,2-Dichloropropane	µg/L	< 500 U	< 1,000 U	< 500 U
cis-1,3-Dichloropropene	µg/L	< 500 U	< 1,000 U	< 500 U
trans-1,3-Dichloropropene	µg/L	< 500 U	< 1,000 U	< 500 U
Ethylbenzene	µg/L	732	< 1,000 U	2,620
2-Hexanone	µg/L	< 2,500 U	< 5,000 U	< 2,500 U
4-Methyl-2-Pentanone (MIBK)	µg/L	< 2,500 U	< 5,000 U	< 2,500 U
Methylene Chloride	µg/L	< 500 U	< 1,000 U	< 500 U
1,1,1,2-Tetrachloroethane	µg/L	< 500 U	< 1,000 U	< 500 U
1,1,2,2-Tetrachloroethane	µg/L	< 500 U	< 1,000 U	< 500 U
Tetrachloroethene	µg/L	< 500 U	< 1,000 U	< 500 U
Toluene	µg/L	49,600	67,100	64,500
Xylenes, Total	µg/L	7,480	4,960	37,400
1,1,1-Trichloroethane	µg/L	< 500 U	< 1,000 U	< 500 U
1,1,2-Trichloroethane	µg/L	< 500 U	< 1,000 U	< 500 U
Trichloroethene	µg/L	< 500 U	< 1,000 U	< 500 U
Vinyl Chloride	µg/L	< 500 U	< 1,000 U	< 500 U
Notes:				

<Blank> Bold deg C mg/L mV/ NA NTU ORP std units </U µg/L

= Not measured

= Analyte Detected

= Degree Celcius

= milligrams per liter

= Microsiemens per Centimeter

= Millivolts

= Standard not available or not currently established

= Nephelometric Turbidity Units

- = Oxidation Reduction Potential
- = Standard units

= Analyte not detected above corresponding Reporting Limit

= micrograms per liter

Table 4

Summary of Previous Groundwater Analytical Results Cell 1: Prototype AS/SVE System in Former Benzol Processing Area Former Coke Oven Area Interim Remedial Measures Severstal Sparrows Point, LLC

	Sample ID Date	CO016-PZM006 7/7/2010	CO-15-PZM005 7/8/2010	CO02-PZM006 7/7/2010	CO02-PZM006 8/25/2010	CO02-PZM006 9/27/2010	CO18-PZM006 7/8/2010	CO18-PZM006 8/25/2010	CO18-PZM006 9/27/2010	BP-MW-09 7/8/2010	BP-MW-09 8/25/2010	BP-MW-09 9/27/2010
Analyte	Units											
Water Quality Parameters	crinto.											-
Temperature	deg C	17.64	17.76	19.67	19,46	20.08	18,20	21,46	22,28	18.21	18,76	20,45
pH	std units	12.51	8,58	8.72	8.06	8,15	7.43	7.25	7.8	12.51	11.32	11.68
ORP	mV	-325	-211	-208	-269	-255	-178	-140	-143	-289	-261	-380
Conductivity	mS/cm	0.772	0.654	0.900	1.220	1.130	0.869	1.520	1.750	1.840	2.270	2.000
Turbidity	NTU	0.1	0.0	0.0	1.5	0.9	0.0	11.3	24.5	0.0	3.8	1.5
DO	mg/L	0.21	0.00	0.00	0.45	0.00	0.00	0.44	0.00	0.00	1.70	0.00
Volatile Organics									•			
Acetone	µg/L	< 50.0 U	< 5,000 U	< 50.0 U	< 5,000 U	< 50.0 U	< 5,000 U	< 5,000 U	< 50.0 U	< 5,000 U	< 5,000 U	< 50.0 U
Benzene	µg/L	176,000	539,000	692,000	441,000	672,000	689,000	941,000	1,010,000	239,000	204,000	221,000
Bromoform	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
2-Butanone	µg/L	< 50.0 U	< 5,000 U	< 50.0 U	< 5,000 U	< 50.0 U	< 5,000 U	< 5,000 U	< 50.0 U	< 5,000 U	< 5,000 U	< 50.0 U
Carbon Disulfide	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
Carbon Tetrachloride	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
Chlorobenzene	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
Chloroethane	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
Chloroform	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
1,1-Dichloroethane	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
1,2-Dichloroethane	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
1,1-Dichlorcethene	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
trans-1,2-Dichlorcethene	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
1,2-Dichloropropane	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
cis-1,3-Dichloropropene	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
trans-1,3-Dichloropropene	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
Ethylbenzene	µg/L	438	1,270	715	786	780	1,050	< 500 U	340	3,420	2,630	2,580
2-Hexanone	µg/L	< 25.0 U	< 2,500 U	< 25.0 U	< 2,500 U	< 25.0 U	< 2,500 U	< 2,500 U	< 25.0 U	< 2,500 U	< 2,500 U	< 25.0 U
4-Methyl-2-Pentanone (MIBK)	µg/L	< 25.0 U	< 2,500 U	< 25.0 U	< 2,500 U	< 25.0 U	< 2,500 U	< 2,500 U	< 25.0 U	< 2,500 U	< 2,500 U	< 25.0 U
Methylene Chloride	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
1,1,1,2-Tetrachloroethane	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
1,1,2,2-Tetrachloroethane	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
Tetrachloroethene	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
Toluene	µg/L	30,200	72,900	82,200	72,800	60,900	77,100	91,000	75,700	75,300	81,100	54,100
Xylenes, Total	µg/L	2,870	9,270	7,610	6,110	6,200	14,100	8,680	5,960	50,300	40,700	36,300
1,1,1-Trichloroethane	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
1,1,2-Trichloroethane	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
Trichloroethene	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U
Vinyl Chloride	µg/L	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U	< 500 U	< 500 U	< 5.0 U

Table 5LNAPL Occurrence and RecoveryCell 6: LNAPL Recovery System in Former Benzol Processing AreaFormer Coke Oven Area Interim Remedial MeasuresSeverstal Sparrows Point, LLC

Well		Total LNAPL R	ecovery Period	Total LNAPL Recovered thru	LNAPL Recovered during October 2010 (gal)	
wen	Occurrence – During October (ft)	Begin	End	October 28, 2010 (gal)		
BP-MW-05	generally about 3	28-Jan	On-going	1,550	166	
RW-04	0.1 to 1.6	23-Jul	On-going	130	61	
BP-MW-08	trace to 2.9	8-Sep	On-going	100	8.2	
BP-MW-11	0.1	23-Jul	8-Sep	7.8	0	
BP-MW-10	0.02	na	na	0	na	
RW-1	0.06 to 0.95	28-Oct	On-going	1	1	
RW-2	0 to 0.21	na	na	0	na	
RW-3	0.16 to 0.34	na	na	0	na	
RW-5	none	na	na	0	na	
BP-MW-07	trace	na	na	0	na	
BP-MW-06	none	na	na	0	na	
BP-MW-09	none	na	na	0	na	
CO19-PZM004	none	na	na	0	na	